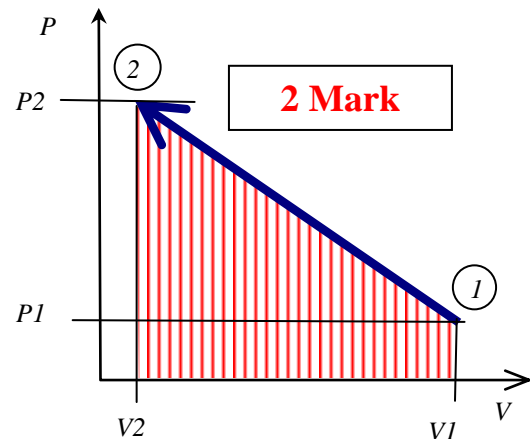
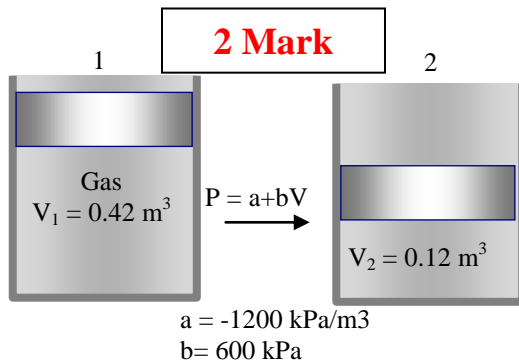


ชื่อ-สกุล.....รหัส..... เลขที่

- 1) A gas is compressed from the initial volume of 0.42 m^3 to the final volume of 0.12 m^3 . During the quasi-equilibrium, the pressure change with the volume according to the relation $P = aV + b$, where V is in m^3 , $a = -1200 \text{ kPa/m}^3$ and $b = 600 \text{ kPa}$.
- Sketch the graph of P-V diagram
 - What is the meaning of area under the P-V relation?
 - Using integrating method, calculate the amount of work during this compression process.

**System:** gas, Closed system**Assumption:** Ideal Gas, neglect ΔKE , ΔPE **1 Mark****Solution**(b) Boundary work: $W = \int P dV$ Therefore, Area under P-V diagram represent ${}_1W_2$

answer

1 Mark

$$(c) \quad {}_1W_2 = \int P dV = \int (aV + b) dV$$

$$= a/2 [V_2^2 - V_1^2] + b[V_2 - V_1]$$

$$a/2 [V_2^2 - V_1^2] = (-1200 \text{ kPa/m}^3)/2 \times [0.12^2 - 0.42^2] = 97.2 \text{ kJ}$$

$$b[V_2 - V_1] = (600 \text{ kPa})(0.12 - 0.42) = -180 \text{ kJ}$$

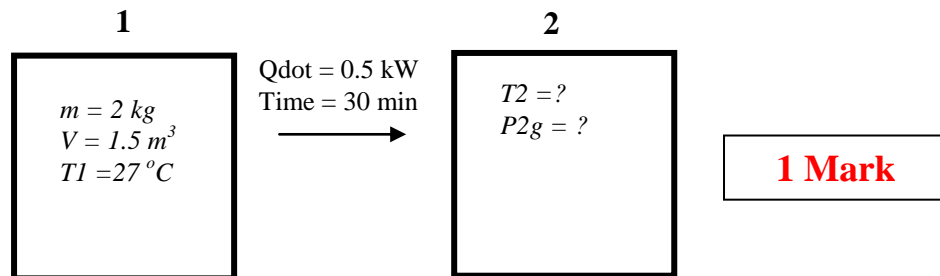
$${}_1W_2 = 97.2 \text{ kJ} - 180 \text{ kJ} = -82.8 \text{ kJ}$$

The work done on the system is 82.8 kJ **Answer****3 Mark****1 Mark**

ชื่อ-สกุล.....รหัส.....เลขที่.....

2) Air of amount 2 kg in a rigid container 1.5 m³ receives heat rate at the amount of 0.5 kW for the period of 30 minutes. The gas constant $R = 0.2870 \text{ kJ/kg}\cdot\text{K}$ and the $C_p = 1.005 \text{ kJ/kg}\cdot\text{K}$ which are constant. The heating process starts with the temperature of the air at $T_1 = 27^\circ\text{C}$. Determine

- a) The final temperature (in the unit of $^\circ\text{C}$).
 b) The value of final pressure (in the form of gage pressure, Pa) if $P_{\text{atm}} = 1 \text{ bar}$.



System: Air, Closed system, Constant volume

Assumption: Ideal gas

1 Mark

Analysis:

1st Law: ${}_1Q_2 = {}_1W_2 + m(u_2 - u_1), \quad {}_1W_2 = 0$
 ${}_1Q_2 = mC_v(T_2 - T_1)$

Relation: $C_p - C_v = R$
 $T_2 = T_1 + {}_1Q_2 / mC_v$

(1)

2 Mark

Heat added, ${}_1Q_2 = Q_{\text{dot}} \times t$

(2)

State 2: $P_2V = mRT_2$

(3)

$P_{2g} = P_2 - P_{\text{atm}}$

(4)

2 Mark

Solution:

$${}_1Q_2 = Q_{\text{dot}} \times t = (0.5 \text{ kW})(30 \text{ min})(60 \text{ s/min})$$

$$= 900 \text{ kJ}$$

$$C_v = C_p - R = (1.005 - 0.287) \text{ kJ/kgK} = 0.718 \text{ kJ/kgK}$$

eqn (1),

$${}_1Q_2 / mC_v = (900 \text{ kJ}) / (2 \text{ kg} \times 0.718 \text{ kJ/kgK}) = 626.7 \text{ K}$$

$$T_2 = T_1 + {}_1Q_2 / mC_p = (27^\circ\text{C} + 273) + 626.7 \text{ K} = 926.7 \text{ K}$$

$$= 653.7^\circ\text{C}$$

Answer

2 Mark

$$P_2 = mRT_2 / V = (2 \text{ kg} \times 0.287 \text{ kJ/kgK} \times 926.7 \text{ K}) / (1.5 \text{ m}^3)$$

$$= 354.7 \text{ kPa}$$

$$= 3.547 \text{ Bar}$$

$$P_{2g} = P_2 - P_{\text{atm}} = (3.547 - 1.0) \text{ Bar} = 2.547 \text{ Bar}$$

$$= 254.7 \text{ kPa}$$

Answer

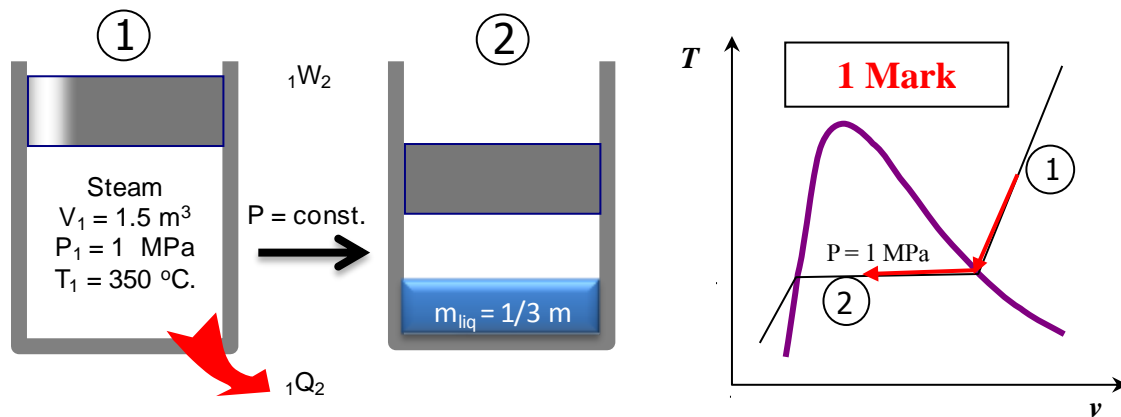
2 Mark

ชื่อ-สกุล.....รหัส.....เลขที่.....

3. A piston-cylinder device contains steam initially at 1 MPa, 350°C, and 1.5 m³. Steam is allowed to cool at constant pressure until one-third of the mass of the steam condensed. Show the process on a T-v diagram with respect to saturation lines (1 mark) and determine,

- (a) the mass of the steam (1 marks)
 (b) the quality (x) at the final state, (1 mark)
 (c) the amount of work during the process, (3 marks)
 (d) the amount of heat transfer. (3 marks)

(การทำงานอย่างเป็นลำดับขั้นตอนที่ดี การเขียนอย่างเรียบร้อยดูง่ายและสะอาด 1 คะแนน)



System Water in the Piston-Cylinder: Closed System: $P = \text{const}$

Assumption Neglect change in KE, PE

Analysis $m = V_1/v_1$
 $-{}_1Q_2$ until $1/2 m$ condensed \rightarrow mixture: $x_2 = m_{\text{vap}}/m$
 ${}_1W_2 = mP_1(v_2 - v_1)$
 ${}_1Q_2 = U_2 - U_1 + {}_1W_2$

Solution

(a) Find mass of the steam:

State 1 $P_1 = 1 \text{ MPa}$, $T_1 = 350^\circ\text{C}$, Table A-5 $T_1 > T_{\text{sat}} \rightarrow$ Superheated vapor

Table A-6 $v_1 = 0.2825 \text{ m}^3/\text{kg}$; $u_1 = 2,875.2 \text{ kJ/kg}$

$$V_1 = 1.5 \text{ m}^3$$

$$m = V_1/v_1 = (1.5 \text{ m}^3)/(0.2825 \text{ m}^3/\text{kg})$$

the mass of steam is 5.31 kg Answer

1 Mark

(b) Find the steam quality

State 2 $P_2 = P_1 = 1 \text{ MPa}$ and $1/3m$ condensed $\rightarrow m_{\text{vap}} = 1/3m$

therefore; quality, $x = m_{\text{vap}}/m = 2/3 = 0.6667$ Answer

1 Mark

(c) **Find Work** : Boundary work: Process $P = c$; ${}_1W_2 = mP_1(v_2 - v_1)$

Table A-5 $v_f = 0.001127 \text{ m}^3/\text{kg}$; $v_g = 0.19444 \text{ m}^3/\text{kg}$

$$v_2 = v_f + xv_g = (0.001127 + 0.6667 \times 0.19444) = 0.1300 \text{ m}^3/\text{kg}$$

$${}_1W_2 = (5.31 \text{ kg})(1000 \text{ kPa})(0.1300 - 0.2825) \text{ m}^3/\text{kg} = -809.7 \text{ kJ}$$

The work done on the system during the process is **809.7 kJ** Answer

3 Mark

(d) Find Heat

1st Law: ${}_1Q_2 = m(u_2 - u_1) + {}_1W_2$

Table A-5 at 1 MPa $u_f = 761.68 \text{ kJ/kg}$; $u_{fg} = 1,822.0 \text{ kJ/kg}$

$$u_2 = u_f + xu_{fg} = (761.68 + 0.6667 \times 1,822.0) = 1,976.3 \text{ kJ/kg}$$

$$m(u_2 - u_1) = (5.31 \text{ kg})(1,976.3 - 2,875.2) \text{ kJ/kg} = -4,772.7 \text{ kJ}$$

then, ${}_1Q_2 = (-4,772.7 \text{ kJ}) + (-809.7 \text{ kJ}) = -5,582.4 \text{ kJ}$

The amount of heat transfer out of the steam is **5,582.4 kJ** Answer

3 Mark

Sommai Priprem

1 Mark

ชื่อ-สกุล.....รหัส.....เลขที่.....

4. Steam flows steadily through a turbine. The inlet conditions of the steam are 15 MPa, 650°C, and 200 m/s, and the exit conditions are 10 kPa, 90 percent quality, and 50 m/s. The mass flow rate of the steam is 150 kg/s. Heat loss from the turbine is 15 kJ/kg steam. State any assumptions made. Show the process on a T-v diagram with respect to saturation line and determine

- (a) the change in kinetic energy,
(b) the power output of the turbine.

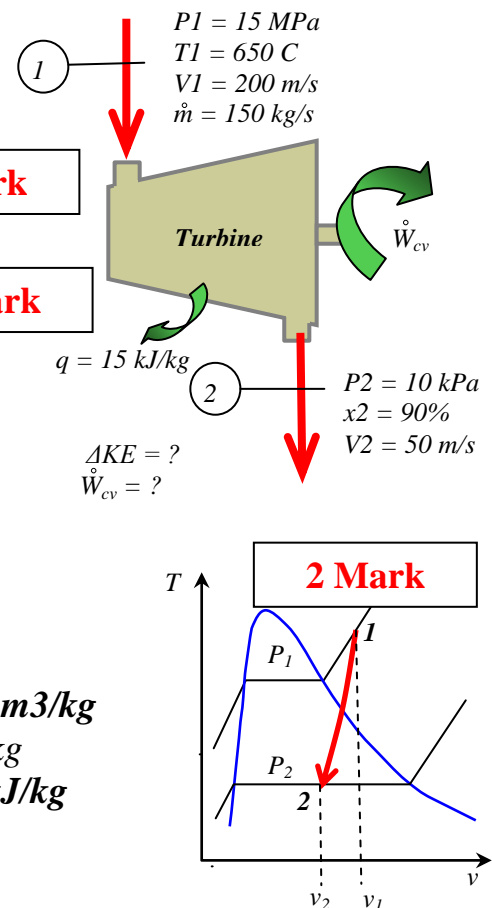
Solution**Assumption:** SSSF process, $\Delta P_E = 0$ **Analysis:**

$$\Delta KE = m(ke_2 - ke_1)$$

$$1st\ law: q + h_1 + ke_1 = w + h_2 + ke_2$$

$$w = q + (h_1 - h_2) - (ke_1 - ke_2)$$

$$W = mw$$

Property:**State 1:** $P_1 = 15\text{ MPa}$, $T_1 = 650\text{ C}$ $T > T_{sat} \rightarrow$ superheat**Table A-6,** $v_1 = 0.0268\text{ m}^3/\text{kg}$ $h_1 = 3,712.30\text{ kJ/kg}$ **State 2:** $P_2 = 10\text{ kPa}$, $x_2 = 90\%$ \rightarrow mixture**Table A-5** $v_f = 0.001452\text{ m}^3/\text{kg}$, $v_g = 0.018026\text{ m}^3/\text{kg}$ $v_2 = v_f + x v_{fg} = 0.0163686\text{ m}^3/\text{kg}$ $h_f = 191.83\text{ kJ/kg}$, $h_{fg} = 2392.8\text{ kJ/kg}$ $h_2 = h_f + x h_{fg} = 2,345.35\text{ kJ/kg}$ **1 Mark****T-v diagram:**State 1 \rightarrow superheated vapor at P_1 State 2 \rightarrow Mixture at P_2 and $v_2 < v_1$ 

$$(a) \quad \Delta KE = m(ke_2 - ke_1)$$

$$(ke_2 - ke_1) = \frac{1}{2} \{ (50\text{ m/s})^2 - (200\text{ m/s})^2 \} / 1000 = -18.75 \quad \text{kJ/kg}$$

$$m = 150\text{ kg/s}$$

$$\Delta KE = m(ke_2 - ke_1) = (150\text{ kg/s})(-18.75\text{ kJ/kg}) = -2,812.50 \quad \text{kW}$$

Change in kinetic energy (decreased) = 2,812.5 kW**Answer****1 Mark**

$$(b) \text{ from eqn 2 } w = q + (h_1 - h_2) - (ke_1 - ke_2)$$

$$q = -15\text{ kJ/kg}$$

$$(h_1 - h_2) = 3712.3\text{ kJ/kg} - 2345.35\text{ kJ/kg}$$

$$= 1367.0\text{ kJ/kg}$$

$$ke_1 - ke_2 = 18.75\text{ kJ/kg}$$

$$w = (-15\text{ kJ/kg}) + (1,367.0\text{ kJ/kg}) - (-18.75\text{ kJ/kg})$$

$$= 1,370.7\text{ kJ/kg}$$

$$W = mw = (150\text{ kg/s})(1,370.7\text{ kJ/kg})$$

$$= 205,605\text{ kW}$$

Power output from the turbine is 205.6 MW**2 Mark****Answer****1 Mark**